



Removal of Sulfur from Gasoline Using Pervaporation: A Review

Abdulaziz A. Alomair*, Yousef Alqaheem

Petroleum Research Center, Kuwait Institute for Scientific Research.

** Corresponding author. Tel.: +965 24956892. Fax: +965 23980445.*

Email address: aomair@kisir.edu.kw

Abstract

Gasoline desulfurization is a vital process in the petroleum industry aimed at reducing the sulfur content in gasoline to meet the updated regulations. Sulfur, a naturally occurring element found in crude oil, poses environmental and health risks when released into the atmosphere during the combustion of gasoline. To address these concerns, desulfurization techniques have been developed to minimize the sulfur content in gasoline, leading to cleaner and more environmentally friendly fuels. Within this context, membrane technology is considered one of the most promising methods for separation applications in several industries including gasoline desulfurization. In this review article, the desulfurization of gasoline using pervaporation (PV) process will be presented in theoretical aspects of material selection and process modification. In addition, parameters such as feed temperature and flow rate are discussed. PV unit has attracted an increasing attention as it provides an effective approach towards an eco-friendly sulfur removal method in petrochemical industries in terms of high selectivity, feasible economics, and safety procedure.

1. Introduction

The combustion of sulfur-containing fuels, such as gasoline, releases sulfur dioxide (SO_2) and nitrogen oxides (NO_x) into the air. These compounds contribute to air pollution, smog formation, and the formation of acid rain [1,2]. Such pollutants have adverse effects on human health, including respiratory problems and increased risk of cardiovascular diseases. Additionally, sulfur compounds can damage emission control systems in vehicles, reducing their effectiveness in reducing harmful emissions [3-6]. To mitigate these issues, gasoline desulfurization plays a crucial role in ensuring compliance with stringent environmental regulations and improving air quality. The process involves the removal of sulfur compounds from gasoline, resulting in cleaner-burning fuels that emit significantly lower levels of harmful pollutants. There are several methods employed for gasoline desulfurization i.e., Hydrodesulfurization (HDS), Adsorbent-based process, Oxidative desulfurization (ODS), Extraction processes, and Catalytic cracking [7]. Hydrodesulfurization (HDS) being the most common. HDS utilizes hydrogen gas (H_2) and a catalyst to facilitate the reaction between sulfur compounds and hydrogen, resulting in the formation of hydrogen sulfide (H_2S) [7-9]. This process effectively reduces the sulfur content in gasoline, making it more environmentally friendly. Adsorptive desulfurization is another technique used in gasoline desulfurization, particularly when extremely low levels of sulfur are required [7, 10]. In this process, adsorbent material is used to selectively adsorb sulfur compounds from gasoline. Commonly used adsorbents include activated carbon, zeolites, and metal oxides [10]. The gasoline is passed through a bed of adsorbent, and the sulfur compounds adhere to the surface of the adsorbent, allowing for their removal. On the other hand, ODS involves the oxidation of sulfur compounds in gasoline to convert them into more polar

compounds that can be easily separated [7,11]. Oxidizing agents, such as hydrogen peroxide or ozone, are used to react with the sulfur compounds and facilitate their removal.

In the extraction processes, various extraction methods can be employed to remove sulfur compounds from gasoline [12,13]. For example, liquid-liquid extraction uses a solvent that selectively extracts sulfur compounds from gasoline. The solvent is then separated from the gasoline, and the sulfur compounds are recovered.

As for the Catalytic cracking processes, such as fluid catalytic cracking (FCC), are primarily used for producing gasoline from crude oil [14-16]. These processes can also help in reducing the sulfur content of gasoline. During catalytic cracking, sulfur compounds are converted into hydrogen sulfide and other gases, which can be separated from the gasoline. Advancements in desulfurization technologies and the implementation of more stringent regulations are driving the development of cleaner and more sustainable fuel options for a greener future [17-22]. Currently, membrane technology has been explored as a potential method for gasoline desulfurization, although it is not as commonly used as other methods such as hydrodesulfurization (HDS) [7-9, 23-25]. Membrane-based desulfurization typically involves the use of selective membranes that can separate sulfur compounds from the gasoline stream. These membranes have specific pore sizes or chemical properties that allow them to selectively permeate sulfur compounds while excluding other gasoline components [26-29]. This process is often referred to as selective permeation. There are different types of membranes that have been investigated for gasoline desulfurization, including polymeric membranes and inorganic membranes [29]. Polymeric membranes are typically made from synthetic polymers, such as polyimides or polymeric blends, and they rely on size exclusion or chemical affinity to separate sulfur compounds. Inorganic membranes, on the other hand, are usually made from ceramic materials, such as zeolites or

metal oxides, and they exploit differences in molecular size or charge to achieve selectivity. One of the potential advantages of membrane-based desulfurization is its ability to operate at ambient conditions, unlike HDS, which requires high temperatures and pressures [30]. This could lead to energy savings and lower operating costs. However, there are several challenges associated with membrane technology, including membrane fouling, low selectivity, and limited scalability. While research and development efforts are ongoing to improve the performance and commercial viability of membrane-based desulfurization, it is important to note that HDS remains the dominant method for gasoline desulfurization in the industry due to its well-established technology and efficiency. However, HDS holds some disadvantages including; the requirement of constant supply of hydrogen gas, which can be expensive [31]. Also, the process operates at high temperatures and pressures, making it energy-intensive. Finally, catalysts used in HDS can be prone to deactivation, leading to reduced efficiency and increased maintenance requirements.

2. Gasoline and sulfur species

Gasoline typically contains trace amounts of sulfur species, primarily as impurities. These sulfur species can be categorized into organic sulfur compounds and inorganic sulfur compounds. Organic and inorganic sulfur compounds are two broad categories of compounds that contain sulfur atoms. Organic sulfur compounds contain carbon-sulfur bonds. In contrast, inorganic sulfur compounds lack carbon-sulfur bonds, and have diverse industrial and environmental applications [32]. The major sulfur compounds are listed in Table 1.

Table 1: Major sulfur compounds in gasoline

Sulfur compounds	Boiling range °C	Sulfur content	
		ppm	%
Mercaptans	66	34	4.5
Thiophene	65-93	37	4.9
C1-thiophenes	92-121	106	14.1
Tetrahydrothiophene	191	24	3.2
C2-thiophenes	120-149	118	15.6
C3-thiophenes/thiophenol	149-190	76	10.1
C4-thiophenes/C1-thiophenol	177	83	11
Benzothiophene	190	276	36.6

2.1 Organic sulfur compounds

Organic sulfur compounds are a class of chemical compounds that contain carbon-sulfur (C-S) bonds. Sulfur is an essential element in organic chemistry, and it plays a crucial role in the structure and function of many biological molecules [29]. Organic sulfur compounds are widespread in nature and can be found in various forms, ranging from simple molecules to complex polymers. Organic sulfur compounds mainly includes, gasoline thiols and disulfides [33]. Gasoline thiols, also known as mercaptans, are a class of organic compounds that contain a sulfur atom bonded to a hydrogen atom (SH group). They are characterized by their strong and unpleasant odor, often described as a "rotten egg" smell. In the context of gasoline, thiols are typically present in small amounts as impurities. Thiols can be formed during the refining and processing of crude oil, which is used to produce gasoline. They can also result from the

degradation of sulfur-containing compounds in the fuel. While modern refining techniques aim to minimize the sulfur content in gasoline, trace amounts of thiols may still be present. The presence of gasoline thiols is undesirable due to their odor, which can be irritating and unpleasant [34,35]. In addition, thiols can contribute to the formation of air pollutants, such as sulfur dioxide and particulate matter, which have negative effects on air quality and human health. To mitigate the presence of thiols in gasoline, various methods are employed, including hydrotreating and catalytic processes during the refining stage. These processes help reduce the sulfur content and remove thiols or convert them to less odorous compounds. It's worth noting that gasoline thiols are different from methyl mercaptan, which is a thiol compound commonly added to odorless natural gas to give it a distinct smell for safety purposes. The addition of methyl mercaptan allows the detection of gas leaks by the characteristic odor [34,36]. On the other hand, gasoline disulfides, also known as sulfur compounds or sulfur-containing compounds in gasoline, refer to organic compounds that contain two sulfur atoms bonded together [37, 38]. They are typically formed by the oxidation of thiols. These compounds are formed during the refining process or can be introduced through various sources, such as crude oil impurities or fuel additives. Disulfides are a subset of sulfur compounds found in gasoline, and they include different chemical species, such as dimethyl disulfide (DMDS), diethyl disulfide (DEDS), and other similar compounds [39, 40]. These compounds contribute to the overall sulfur content of gasoline, which is regulated in many countries due to environmental concerns. The presence of disulfides in gasoline can have several effects including emissions, catalyst poisoning and odor.

- Emissions: Sulfur compounds in gasoline can contribute to the emission of sulfur dioxide (SO_2) and other sulfur-containing pollutants when the fuel is burned. These pollutants are

known to be harmful to human health and the environment, contributing to air pollution, acid rain, and respiratory issues.

- Catalyst poisoning: Sulfur compounds can poison catalytic converters used in vehicle exhaust systems. These converters are designed to reduce emissions of pollutants like nitrogen oxides (NO_x) and carbon monoxide (CO). The sulfur compounds can interact with the catalyst, reducing its efficiency and leading to increased emissions.
- Odor: Some sulfur compounds, such as DMDS, have a distinct odor, which can contribute to the unpleasant smell associated with gasoline.

2.2 Inorganic sulfur compounds

Inorganic sulfur compounds can be present in gasoline as impurities or as additives. These compounds are typically sulfur-containing chemicals that are not derived from crude oil but are introduced during the refining or blending process [41]. One common inorganic sulfur compound found in gasoline is hydrogen sulfide (H₂S). H₂S is a colorless gas with a distinct rotten egg smell and is highly toxic. It is usually removed during the refining process to prevent its release into the atmosphere. Other inorganic sulfur compounds that may be present in gasoline include sulfur dioxide (SO₂) and sulfur trioxide (SO₃). These compounds can be formed during the combustion of gasoline and contribute to air pollution, leading to the formation of acid rain and the exacerbation of respiratory problems [42].

3. Sulfur removal from FCC gasoline using PV

Fluid catalytic cracking is a widely used refining process in the petroleum industry to convert heavy hydrocarbon feedstocks into lighter, more valuable products such as gasoline and diesel [43,44]. However, one of the challenges associated with FCC is the presence of sulfur compounds in the products, which are undesirable due to their detrimental effects on the

environment and catalytic activity [45-48]. Pervaporation offers an effective solution for removing sulfur from FCC products.

3.1 Basics of PV

Pervaporation is a membrane separation process used to separate liquid mixtures based on their vapor pressure differences [49-55]. In pervaporation, a liquid mixture is brought into contact with a selective membrane, and a partial vacuum is applied on one side of the membrane as illustrated in Figure 1. As a result, one component of the liquid mixture selectively permeates through the membrane as vapor, while the other components remain behind as a concentrated liquid or retentate [55]. The driving force behind pervaporation is the vapor pressure difference between the components of the liquid mixture. The membrane used in pervaporation is typically a thin, selective layer that allows the preferential transport of one component while rejecting the others. The selective layer can be made of various materials, including polymers, ceramics, or composite materials. The permeated vapor is collected on the other side of the membrane, where it can be condensed and separated from the permeate. The permeate usually contains a higher concentration of the more volatile component of the liquid mixture. The retentate, on the other hand, becomes more concentrated in the less volatile component. Pervaporation has several advantages over traditional separation processes such as distillation or absorption. It operates at lower temperatures and pressures, making it more energy-efficient. It is particularly useful for separating azeotropic or close-boiling mixtures that are difficult to separate by conventional means. Pervaporation is also effective for removing volatile organic compounds from water or solvents. Applications of pervaporation include the dehydration of organic solvents, the removal of water from organic compounds, the recovery of organic solvents, and the purification of

specialty chemicals. It is also used in the food and beverage industry for the concentration of fruit juices and the removal of alcohol from beverages. Currently, pervaporation is being used in removing sulfur from fluid catalytic cracking (FCC) products [55-59].

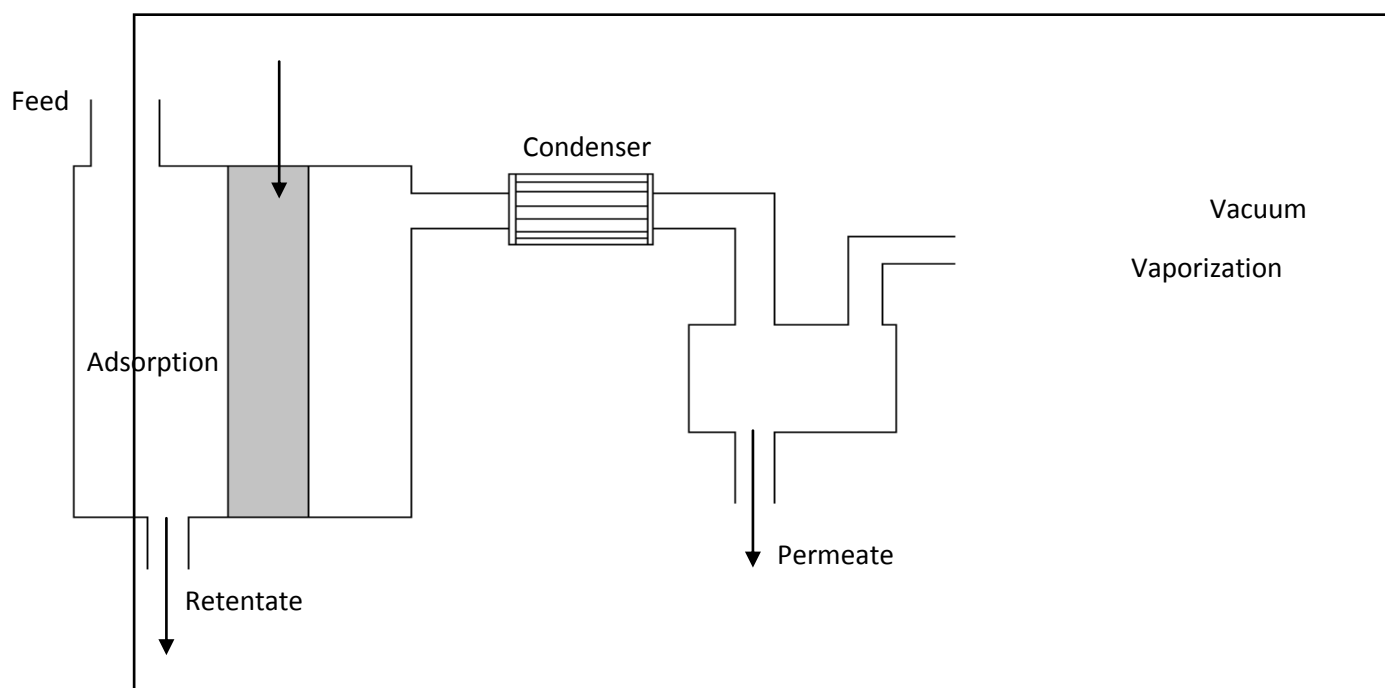


Figure. 1. Schematic diagram on gasoline desulfurization using PV.

3.2 PV process and operation

The process involves passing the FCC products through a membrane that selectively permeates sulfur compounds, allowing them to be separated from the desired hydrocarbons [57]. The membrane used in pervaporation is typically made of a polymer material with high sulfur selectivity [60]. During pervaporation, the FCC product mixture is heated and brought into contact with one side of the membrane. The sulfur compounds present in the mixture have higher

affinity and permeability through the membrane compared to hydrocarbons. As a result, sulfur compounds preferentially permeate through the membrane, while hydrocarbons are retained on the feed side. The permeated sulfur compounds can be collected and further treated or processed to recover valuable sulfur or disposed of in an environmentally friendly manner. The purified hydrocarbon stream is obtained from the feed side of the membrane, free from significant amounts of sulfur compounds. Pervaporation for sulfur removal from FCC products offers several advantages. It operates at relatively mild conditions, requiring moderate temperatures and pressures, which can reduce energy consumption compared to conventional sulfur removal methods. Additionally, pervaporation is a continuous process and can be integrated into existing FCC units, making it a potentially cost-effective solution [61,62]. However, it's important to note that pervaporation for sulfur removal is still a developing technology, and there may be challenges related to membrane fouling, membrane selectivity, and overall process efficiency [63]. Research and development efforts are ongoing to optimize membrane materials and process parameters to enhance the performance and commercial viability of pervaporation for sulfur removal in FCC applications.

4. Materials selection

The selection of membrane materials for pervaporation process in FCC gasoline desulfurization depends on several factors, including the desired separation performance, chemical compatibility, stability, and cost-effectiveness. Materials such as zeolites, polymers, and biological materials have been applied as membranes for this application [64-66]. Table 2 presents the PV membrane materials reported recently and their sulfur removal performance.

Table 2: Comparison of the separation efficiencies of various membranes.

Membrane	Sulfur Content, ppm	Temperature, °C	Flux, (J, kg/m ² h)	Separation factor	Reference
UF G - 10	4239	-	0.45	53.61	67
PI	248	71	6.2	2.18	68
PDMS-Ag ₂ O/PAN	3640	30	1.65	3.9	69
PDMS-AgY/PAN	3700	31	1.04	4.4	70
PDMS/ ceramic	1000	50	3.31	3.35	71
PEG/PES	1300	33	6.95	3.15	72
EC	300	80	0.7	3.75	73
PBPP	400	55	0.038	11.92	74
CI-PBPP	400	85	1.38	5.6	75
PEBA / PVDF	1000	40	3.8	4	76
PDMS-GNS	1312	40	6.22	3.58	77

Nevertheless, polymers are currently the most broadly used materials [78 – 82] due to the fact that polymer materials offer several advantages over other materials when it comes to membranes including;

- Versatility: Polymer membranes can be designed to have a wide range of properties, making them highly versatile. They can be tailored to have specific pore sizes, surface chemistries, and permeability characteristics to suit various applications [79,83].

- **Selectivity:** Polymer membranes can exhibit excellent selectivity, allowing them to separate specific molecules or ions from a mixture. By controlling the polymer composition and structure, it is possible to achieve high selectivity for a particular substance, which is crucial in applications such as water purification, gas separation, and drug delivery [78].
- **Scalability:** Polymer membranes are often more scalable than other materials, such as ceramic or metal membranes. They can be manufactured through various techniques, including phase inversion, electrospinning, and casting, which are relatively cost-effective and suitable for large-scale production [81].
- **Energy Efficiency:** Polymer membranes can offer high permeability with low energy consumption, making them energy-efficient. They can enable efficient separation processes by requiring less pressure or lower temperature differentials compared to other membrane materials. This is particularly important in applications like reverse osmosis for desalination or gas separation for industrial processes [82,84].
- **Chemical Resistance:** Many polymer materials exhibit excellent chemical resistance, allowing them to withstand exposure to harsh chemicals, acids, and solvents without significant degradation. This makes them suitable for applications in corrosive environments or when dealing with aggressive substances [78-85].
- **Flexibility and Ease of Processing:** Polymer membranes are typically flexible and can be easily formed into various shapes or configurations, including flat sheets, hollow fibers, or tubular structures. Their flexibility enables their use in applications where conformability or flexibility is required, such as in wearable devices or flexible electronics [86].
- **Cost-Effectiveness:** Polymer membranes are often more cost-effective compared to other membrane materials, such as ceramics or metals. The raw materials for polymers are relatively

inexpensive, and the manufacturing processes can be less complex and more cost-efficient, resulting in lower production costs [87].

5. Effect of the gasoline components on membranes performance

The effect of gasoline on a polymer membrane can vary depending on the specific polymer composition and the exposure conditions [88,90]. When gasoline comes into contact with a polymer membrane, several potential interactions can occur including; swelling, solvent action, Permeation and Chemical degradation. Some polymers may absorb gasoline and swell as a result. This can lead to changes in the dimensions and mechanical properties of the membrane. Also, gasoline can act as a solvent for certain polymers, causing them to dissolve or soften. This can lead to a loss of structural integrity and a breakdown of the membrane. Gasoline molecules may diffuse through the polymer membrane, leading to permeation [91]. This can be problematic in applications where the membrane is intended to provide a barrier against the passage of liquids. Chemical degradation can take place because the aromatic components of gasoline can chemically react with certain polymer materials, resulting in degradation of the polymer chains. This can lead to a loss of mechanical strength, embrittlement, or cracking of the membrane. To mitigate the potential negative effects of gasoline on a polymer membrane [92], various strategies can be employed. These include selecting a polymer material with high resistance to gasoline, using barrier coatings or laminates to protect the membrane, or incorporating additives that enhance resistance to gasoline exposure [93,94]. It is important to consider the specific

requirements of the application and consult the manufacturer's recommendations or conduct appropriate testing to ensure the compatibility of the polymer membrane with gasoline [95].

6. Operating parameters

The operating conditions in pervaporation can significantly influence its performance. Here are some key factors:

6.1 Effect of feed temperature

Pervaporation is a temperature-dependent process [96]. As temperature increases, the vapor pressure of the components in the liquid mixture also increases, resulting in enhanced permeation rates as illustrated by Arrhenius relationship (Figure 2) [96,97]. In addition, higher temperatures accelerate the diffusion rate of solutes in the solution [98]. This increased molecular motion results in a greater concentration gradient across the membrane, leading to enhanced mass transfer through the membrane and consequently higher flux [99]. Moreover, the permeability of the membrane itself can be influenced by temperature. In some cases, higher temperatures can reduce the resistance of the membrane, leading to increased permeability and flux [100]. For example in polymeric membranes, the polymer chains become flexible at higher temperatures, resulting more available free volume and paths within the membrane structure. However, the selectivity of the membrane may decrease at higher temperatures due to increased diffusion of both components. Therefore, an optimal temperature must be selected to achieve the desired separation performance.

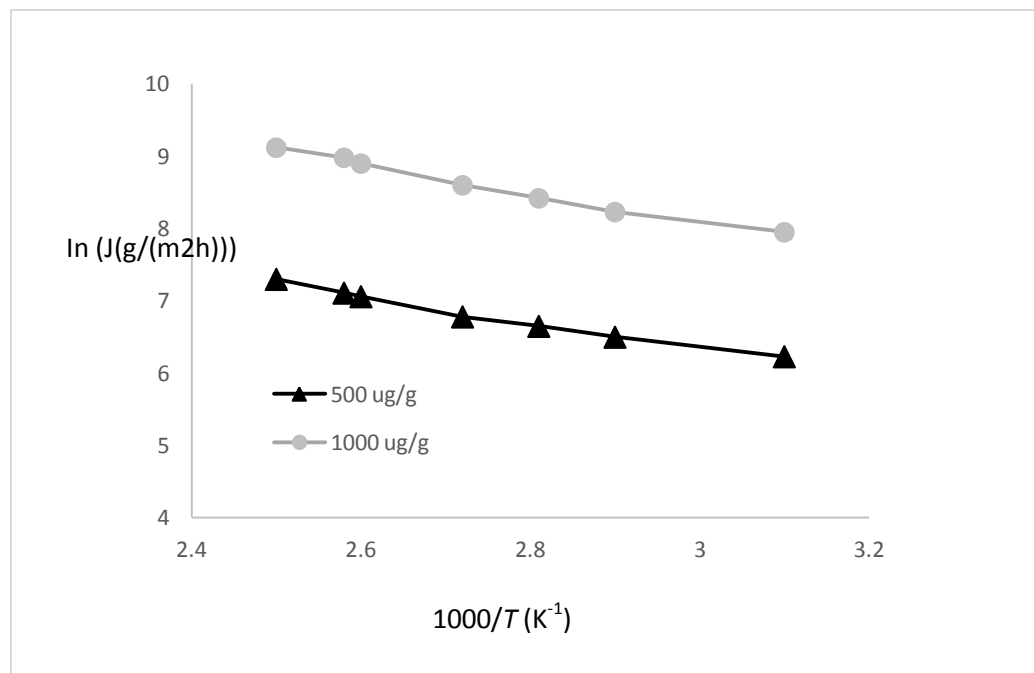


Figure 2: Arrhenius relationship between flux and temperature [70].

6.2 Effect of feed pressures

Feed pressure is an important operational parameter that can significantly affect the performance of a pervaporation membrane system used for separating gasoline components [101]. The feed pressure in a pervaporation system affects the separation performance in several ways:

1. Permeation Flux: Generally, increasing the feed pressure in a pervaporation system leads to an increase in the permeation flux. Higher pressure can enhance the driving force for mass transfer across the membrane, resulting in increased permeation rates. This can be beneficial for achieving higher separation efficiency and higher productivity [102, 103].

2. Selectivity: Feed pressure can influence the selectivity of the membrane system. In some cases, high feed pressures can cause a reduction in selectivity, leading to increased co-permeation of undesired components. This can result in lower separation efficiency and reduced product quality [102-104].

3. Membrane Performance: Pervaporation membranes have certain operating limits, including pressure differentials, beyond which their performance may deteriorate or they may be damaged [105]. Excessive feed pressures can cause membrane compaction, increased mechanical stresses, or even membrane rupture, leading to a loss in separation efficiency and membrane integrity [102, 106]. It is important to operate the pervaporation system within the recommended pressure range specified by the membrane manufacturer.

6.3 Effect of feed composition

Specific effects of gasoline on a membrane will depend on factors such as the membrane composition, thickness, exposure duration, and the concentration and composition of the gasoline itself [107]. Different types of membranes may exhibit different responses to gasoline exposure. Gasoline contains a mixture of hydrocarbons, some of which can be chemically reactive. Prolonged exposure to gasoline can lead to chemical degradation of the membrane material [108]. This degradation can result in changes to the membrane's structure, loss of mechanical strength, and reduced performance. In addition, gasoline may cause the leaching of certain additives or plasticizers present in the membrane material. This leaching can alter the membrane's properties and potentially contaminate the surrounding environment.

6.4 Influence of feed sulfur concentration

Sulfur compounds, especially inorganic sulfates and sulfides, can cause fouling on the membrane surface. Fouling refers to the accumulation of unwanted substances on the membrane, which can reduce its performance and efficiency [109]. Sulfur fouling can be particularly problematic because sulfur compounds tend to form insoluble precipitates that adhere to the membrane surface. Other sulfur compounds, such as hydrogen sulfide (H₂S), can react with the membrane material and cause degradation. This degradation may result in changes in membrane morphology, reduced mechanical strength, and increased susceptibility to fouling and chemical attack [109,110].

6.5 Effect of feed flow rate

The gasoline feed flow rate can have several effects on a membrane system. The feed flow rate will generally lead to higher permeate flux. However, there is a limit to this relationship as excessively high flow rates can result in reduced efficiency due to limitations in the membrane's permeability and fouling resistance [111]. Also, higher feed flow rates can help to minimize fouling by promoting a higher shear rate and maintaining a more turbulent flow. This can help prevent the deposition of particles on the membrane surface and improve overall efficiency. Another aspect that should be considered is the pressure drop. The feed flow rate is directly related to the pressure drop across the membrane system. Increasing the flow rate will generally lead to a higher pressure drop [111,112]. The feed flow rate can impact the energy consumption of the membrane system. Higher flow rates typically require more energy to maintain the desired pressure and flow conditions. Therefore, it is important to consider the energy requirements and

cost-effectiveness when determining the optimal feed flow rate. Also, The feed flow rate can also affect the lifespan and durability of the membrane. Operating at excessively high flow rates for extended periods may result in increased mechanical stress on the membrane, potentially leading to damage or reduced membrane lifespan. It is important to operate within the recommended operating conditions specified by the membrane manufacturer to ensure longevity.

7. Economic analysis

Pervaporation is a membrane separation process that has been explored for various applications, including the desulfurization of gasoline. The economic analysis of pervaporation for gasoline desulfurization involves evaluating the costs and benefits associated with implementing this technology. Here are some key factors to consider in such an analysis. The capital costs are the initial investment required to set up a pervaporation system for gasoline desulfurization includes the cost of purchasing and installing the pervaporation membranes, pumps, and other equipment. These costs can vary depending on the scale of the operation and the specific membrane materials used. As for the operating costs of a pervaporation system include energy consumption, maintenance, and replacement of membranes [113, 114]. Energy costs will depend on the power requirements of the pumps and other equipment. Membrane replacement is necessary over time due to fouling or degradation, and the frequency and cost of replacement will impact the overall operating costs. In general, the effectiveness of pervaporation in removing sulfur compounds from gasoline will influence the economic analysis. Higher sulfur removal efficiency means a higher-quality desulfurized product, which may command a premium price in the market. The quality of the desulfurized gasoline product produced through pervaporation will play a significant role in the economic analysis. If the desulfurized gasoline meets the regulatory

standards and has desirable properties, its market value may be higher compared to conventional gasoline. The cost of the gasoline feedstock is an important consideration. If the pervaporation process allows for the use of lower-cost, high-sulfur feedstocks, it can provide a cost advantage compared to alternative desulfurization methods that require more expensive low-sulfur feedstocks. Environmental regulations regarding sulfur content in gasoline can impact the economic analysis. If pervaporation enables compliance with stricter regulations at a lower cost compared to alternative technologies, it can provide a competitive advantage. On the other hand, the scale at which the pervaporation system is implemented can affect the economics. Large-scale operations may benefit from economies of scale, potentially reducing capital and operating costs per unit of desulfurized gasoline produced.

8. Final remarks and future prospects

In conclusion, gasoline desulfurization using pervaporation has proven to be a promising technology for the removal of sulfur compounds from gasoline. It offers several advantages over conventional methods, such as higher selectivity, lower energy consumption, and simpler operation. Pervaporation has demonstrated its efficiency in removing both organic and inorganic sulfur compounds, including difficult-to-remove compounds like thiophene and benzothiophene. The use of selective membranes in pervaporation enables the separation of sulfur compounds from gasoline based on their molecular size, polarity, and affinity to the membrane material. By optimizing the membrane properties and operating conditions, high desulfurization efficiency can be achieved while maintaining a high gasoline recovery rate. As for the future prospects, continued research and development efforts should focus on designing and optimizing membranes specifically tailored for gasoline desulfurization. This includes improving the

selectivity, permeability, and stability of the membranes to enhance their performance and longevity. Also, Pervaporation can be integrated with other desulfurization technologies, such as hydrotreating or adsorption, to create hybrid processes that offer synergistic benefits. The combination of different technologies can potentially enhance the overall desulfurization efficiency and reduce operating costs. While pervaporation has shown promise at the laboratory scale, further efforts are needed to scale up the technology for industrial applications. The development of large-scale pervaporation systems and the evaluation of their economic feasibility will be crucial steps towards commercialization.

References

- 1- Saleh, T.A., 2020. Characterization, determination and elimination technologies for sulfur from petroleum: Toward cleaner fuel and a safe environment. *Trends in Environmental Analytical Chemistry*, 25, p.e00080.
- 2- Alyassiry, A.A. and Alrubaye, R.T.A., 2020, March. Desulfurization of model gasoline using metal organic frame-work. In *AIP Conference Proceedings* (Vol. 2213, No. 1). AIP Publishing.
- 3- Liu, H., Wang, X., Zhang, D., Dong, F., Liu, X., Yang, Y., Huang, H., Wang, Y., Wang, Q. and Zheng, Z., 2019. Investigation on blending effects of gasoline fuel with n-butanol, DMF, and ethanol on the fuel consumption and harmful emissions in a GDI vehicle. *Energies*, 12(10), p.1845.
- 4- Domingo, J.L. and Rovira, J., 2020. Effects of air pollutants on the transmission and severity of respiratory viral infections. *Environmental research*, 187, p.109650.
- 5- Patel, N., Khan, M.D., Shahane, S., Rai, D., Chauhan, D., Kant, C. and Chaudhary, V.K., 2020. Emerging pollutants in aquatic environment: source, effect, and challenges in biomonitoring and bioremediation-a review. *Pollution*, 6(1), pp.99-113.
- 6- Cheng, X., Shi, Z., Glass, N., Zhang, L., Zhang, J., Song, D., Liu, Z.S., Wang, H. and Shen, J., 2007. A review of PEM hydrogen fuel cell contamination: Impacts, mechanisms, and mitigation. *Journal of Power Sources*, 165(2), pp.739-756.
- 7- Saha, B., Vedachalam, S. and Dalai, A.K., 2021. Review on recent advances in adsorptive desulfurization. *Fuel Processing Technology*, 214, p.106685.

- 8- Brunet, S., Mey, D., Pérot, G., Bouchy, C. and Diehl, F., 2005. On the hydrodesulfurization of FCC gasoline: a review. *Applied Catalysis A: General*, 278(2), pp.143-172.
- 9- Toba, M., Miki, Y., Matsui, T., Harada, M. and Yoshimura, Y., 2007. Reactivity of olefins in the hydrodesulfurization of FCC gasoline over CoMo sulfide catalyst. *Applied Catalysis B: Environmental*, 70(1-4), pp.542-547.
- 10- Ganiyu, S.A. and Lateef, S.A., 2021. Review of adsorptive desulfurization process: Overview of the non-carbonaceous materials, mechanism and synthesis strategies. *Fuel*, 294, p.120273.
- 11- Mjalli, F.S., Ahmed, O.U., Al-Wahaibi, T., Al-Wahaibi, Y. and AlNashef, I.M., 2014. Deep oxidative desulfurization of liquid fuels. *Reviews in Chemical Engineering*, 30(4), pp.337-378.
- 12- Alonso, L., Arce, A., Francisco, M., Rodríguez, O. and Soto, A., 2007. Gasoline desulfurization using extraction with [C8mim][BF₄] ionic liquid. *AIChE Journal*, 53(12), pp.3108-3115.
- 13- Yin, J., Wang, J., Li, Z., Li, D., Yang, G., Cui, Y., Wang, A. and Li, C., 2015. Deep desulfurization of fuels based on an oxidation/extraction process with acidic deep eutectic solvents. *Green Chemistry*, 17(9), pp.4552-4559.
- 14- Wen, Y., Wang, G., Xu, C. and Gao, J., 2012. Study on in situ sulfur removal from gasoline in fluid catalytic cracking process. *Energy & fuels*, 26(6), pp.3201-3211.
- 15- Cheng, W.C., Kim, G., Peters, A.W., Zhao, X., Rajagopalan, K., Ziebarth, M.S. and Pereira, C.J., 1998. Environmental fluid catalytic cracking technology. *Catalysis Reviews*, 40(1-2), pp.39-79.
- 16- Ong, Y.K. and Bhatia, S., 2010. The current status and perspectives of biofuel production via catalytic cracking of edible and non-edible oils. *Energy*, 35(1), pp.111-119.
- 17- Li, X., Han, J., Liu, Y., Dou, Z. and Zhang, T.A., 2022. Summary of research progress on industrial flue gas desulfurization technology. *Separation and Purification Technology*, 281, p.119849.
- 18- Srivastava, V.C., 2012. An evaluation of desulfurization technologies for sulfur removal from liquid fuels. *Rsc Advances*, 2(3), pp.759-783.
- 19- Lam, V., Li, G., Song, C., Chen, J., Fairbridge, C., Hui, R. and Zhang, J., 2012. A review of electrochemical desulfurization technologies for fossil fuels. *Fuel processing technology*, 98, pp.30-38.
- 20- Babich, I.V. and Moulijn, J.A., 2003. Science and technology of novel processes for deep desulfurization of oil refinery streams: a review☆. *Fuel*, 82(6), pp.607-631.
- 21- Song, C. and Ma, X., 2009. Desulfurization technologies. *Hydrogen and syngas production and purification technologies*, pp.219-310.

- 22- Esmaeili-Faraj, S.H., Hassanzadeh, A., Shakeriankhoo, F., Hosseini, S. and Vaferi, B., 2021. Diesel fuel desulfurization by alumina/polymer nanocomposite membrane: Experimental analysis and modeling by the response surface methodology. *Chemical Engineering and Processing-Process Intensification*, 164, p.108396.
- 23- Han, X., Sun, H., Liu, L., Wang, Y., He, G. and Li, J., 2019. Improved desulfurization performance of polydimethylsiloxane membrane by incorporating metal organic framework CPO-27-Ni. *Separation and Purification Technology*, 217, pp.86-94.
- 24- Ahmad, W., 2016. Sulfur in petroleum: petroleum desulfurization techniques. In *Applying nanotechnology to the desulfurization process in petroleum engineering* (pp. 1-52). IGI Global.
- 25- Liu, K., Fang, C.J., Li, Z.Q. and Young, M., 2014. Separation of thiophene/n-heptane mixtures using PEBAX/PVDF-composited membranes via pervaporation. *Journal of membrane science*, 451, pp.24-31.
- 26- Li, B., Xu, D., Jiang, Z., Zhang, X., Liu, W. and Dong, X., 2008. Pervaporation performance of PDMS-Ni²⁺ Y zeolite hybrid membranes in the desulfurization of gasoline. *Journal of Membrane Science*, 322(2), pp.293-301.
- 27- Li, B., Liu, W., Wu, H., Yu, S., Cao, R. and Jiang, Z., 2012. Desulfurization of model gasoline by bioinspired oleophilic nanocomposite membranes. *Journal of membrane science*, 415, pp.278-287.
- 28- Liu, Y., Feng, X. and Lawless, D., 2006. Separation of gasoline vapor from nitrogen by hollow fiber composite membranes for VOC emission control. *Journal of Membrane Science*, 271(1-2), pp.114-124.
- 29- Fihri, A., Mahfouz, R., Shahrani, A., Taie, I. and Alabedi, G., 2016. Pervaporative desulfurization of gasoline: a review. *Chemical Engineering and Processing-Process Intensification*, 107, pp.94-105.
- 30- Cotet, L.C., Magyari, K., Todea, M., Dulescu, M.C., Danciu, V. and Baia, L., 2017. Versatile self-assembled graphene oxide membranes obtained under ambient conditions by using a water-ethanol suspension. *Journal of Materials Chemistry A*, 5(5), pp.2132-2142.
- 31- Kabe, T., Ishihara, A. and Qian, W., 1999. Hydrodesulfurization and hydrodenitrogenation. *Chemistry and Engineering*.
- 32- Docter, A. and Lamm, A., 1999. Gasoline fuel cell systems. *Journal of Power Sources*, 84(2), pp.194-200.
- 33- Kharasch, N. ed., 2013. *Organic sulfur compounds*. Elsevier.
- 34- Ndagijimana, P., Liu, X., Li, Z., Xing, Z., Pan, B., Yu, G. and Wang, Y., 2021. Adsorption performance and mechanisms of mercaptans removal from gasoline oil using core-shell AC-based adsorbents. *Environmental Science and Pollution Research*, 28, pp.67120-67136.

- 35- Lei, W., Dasgupta, P.K., Matza, S.D. and Olson, D.C., 1989. Measurement of mercaptans in gasoline. *Microchimica Acta*, 99, pp.35-41.
- 36- Yang, C., Yu, J., Huang, B., Miao, G. and Xiao, J., 2023. Boosting deep desulfurization of heavy mercaptan using layered intercalated Zn-based hydroxide adsorbents. *Separation and Purification Technology*, 307, p.122860.
- 37- Sakr, A.A.E., Amr, N., Bakry, M., El-Azab, W.I. and Ebiad, M.A., 2023. Carbon disulfide removal from gasoline fraction using zinc-carbon composite synthesized using microwave-assisted homogenous precipitation. *Environmental Science and Pollution Research*, pp.1-17.
- 38- Miki, Y., Toba, M. and Yoshimura, Y., 2008. Analysis of sulfur compounds in straight-run naphtha and FCC gasoline. *Journal of the Japan Petroleum Institute*, 51(4), pp.225-233.
- 39- Giri, B.S., Kim, K.H., Pandey, R.A., Cho, J., Song, H. and Kim, Y.S., 2014. Review of biotreatment techniques for volatile sulfur compounds with an emphasis on dimethyl sulfide. *Process Biochemistry*, 49(9), pp.1543-1554.
- 40- Srivastava, R.K., Miller, C.A., Erickson, C. and Jambhekar, R., 2004. Emissions of sulfur trioxide from coal-fired power plants. *Journal of the Air & Waste Management Association*, 54(6), pp.750-762.
- 41- Borisov, S.V.E., Magarill, S.A. and Pervukhina, N.Y.V., 2015. Crystallographic analysis of a series of inorganic compounds. *Russian Chemical Reviews*, 84(4), p.393.
- 42- Costa, J.A.S., de Jesus, R.A., Santos, D.O., Mano, J.F., Romao, L.P. and Paranhos, C.M., 2020. Recent progresses in the adsorption of organic, inorganic, and gas compounds by MCM-41-based mesoporous materials. *Microporous and Mesoporous Materials*, 291, p.109698.
- 43- Vogt, E.T. and Weckhuysen, B.M., 2015. Fluid catalytic cracking: recent developments on the grand old lady of zeolite catalysis. *Chemical Society Reviews*, 44(20), pp.7342-7370.
- 44- Bai, P., Etim, U.J., Yan, Z., Mintova, S., Zhang, Z., Zhong, Z. and Gao, X., 2019. Fluid catalytic cracking technology: current status and recent discoveries on catalyst contamination. *Catalysis Reviews*, 61(3), pp.333-405.
- 45- Sadeghbeigi, R., 2020. *Fluid catalytic cracking handbook: An expert guide to the practical operation, design, and optimization of FCC units*. Butterworth-Heinemann.
- 46- Pujro, R., Falco, M. and Sedran, U., 2015. Catalytic cracking of heavy aromatics and polycyclic aromatic hydrocarbons over fluidized catalytic cracking catalysts. *Energy & Fuels*, 29(3), pp.1543-1549.
- 47- Pinheiro, C.I., Fernandes, J.L., Domingues, L., Chambel, A.J., Graca, I., Oliveira, N.M., Cerqueira, H.S. and Ribeiro, F.R., 2012. Fluid catalytic cracking (FCC) process

- modeling, simulation, and control. *Industrial & engineering chemistry research*, 51(1), pp.1-29.
- 48- Magee, J.S. and Mitchell, M.M. eds., 1993. *Fluid catalytic cracking: science and technology*. Elsevier.
- 49- Feng, X. and Huang, R.Y., 1997. Liquid separation by membrane pervaporation: a review. *Industrial & Engineering Chemistry Research*, 36(4), pp.1048-1066.
- 50- Smitha, B., Suhanya, D., Sridhar, S. and Ramakrishna, M., 2004. Separation of organic–organic mixtures by pervaporation—a review. *Journal of membrane science*, 241(1), pp.1-21.
- 51- Cheng, X., Pan, F., Wang, M., Li, W., Song, Y., Liu, G., Yang, H., Gao, B., Wu, H. and Jiang, Z., 2017. Hybrid membranes for pervaporation separations. *Journal of Membrane Science*, 541, pp.329-346.
- 52- Prihatiningtyas, I. and Van der Bruggen, B., 2020. Nanocomposite pervaporation membrane for desalination. *Chemical Engineering Research and Design*, 164, pp.147-161.
- 53- Vane, L.M., 2020. Review of pervaporation and vapor permeation process factors affecting the removal of water from industrial solvents. *Journal of Chemical Technology & Biotechnology*, 95(3), pp.495-512.
- 54- Castro-Muñoz, R., 2020. Breakthroughs on tailoring pervaporation membranes for water desalination: A review. *Water research*, 187, p.116428.
- 55- Alomair, A.A., Al-Jubouri, S.M. and Holmes, S.M., 2015. A novel approach to fabricate zeolite membranes for pervaporation processes. *Journal of Materials Chemistry A*, 3(18), pp.9799-9806.
- 56- Mishra, M.K. and Jain, M., 2021. Removal of sulfur-containing compounds from Fluid Catalytic Cracking unit (FCC) gasoline by pervaporation process: Effects of variations in feed characteristics and mass transfer properties of the membrane. *Asia-Pacific Journal of Chemical Engineering*, 16(4), p.e2653.
- 57- Jain, M., Attarde, D. and Gupta, S.K., 2017. Removal of thiophenes from FCC gasoline by using a hollow fiber pervaporation module: Modeling, validation, and influence of module dimensions and flow directions. *Chemical Engineering Journal*, 308, pp.632-648.
- 58- Jain, M., 2016. Separation of sulfur compounds from FCC gasoline by pervaporation (Doctoral dissertation, IIT Delhi).
- 59- Chen, J., Li, J., Qi, R., Ye, H. and Chen, C., 2008. Pervaporation performance of crosslinked polydimethylsiloxane membranes for deep desulfurization of FCC gasoline: I. Effect of different sulfur species. *Journal of Membrane Science*, 322(1), pp.113-121.
- 60- Lin, L., Zhang, Y. and Kong, Y., 2009. Recent advances in sulfur removal from gasoline by pervaporation. *Fuel*, 88(10), pp.1799-1809.

- 61- White, L.S., 2006. Development of large-scale applications in organic solvent nanofiltration and pervaporation for chemical and refining processes. *Journal of Membrane Science*, 286(1-2), pp.26-35.
- 62- Qi, R., Wang, Y., Li, J. and Zhu, S., 2006. Sulfur removal from gasoline by pervaporation: The effect of hydrocarbon species. *Separation and purification technology*, 51(3), pp.258-264.
- 63- Lu, H.X., Bu, S.F. and Wang, Z.P., 2014. Removal of sulfur from MTBE by pervaporation process. *Applied Mechanics and Materials*, 521, pp.617-620.
- 64- Chern, R.T., Koros, W.J., Hopfenberg, H.B. and Stannett, V.T., 1985. Material selection for membrane-based gas separations.
- 65- Nunes, S.P., Culfaz-Emecen, P.Z., Ramon, G.Z., Visser, T., Koops, G.H., Jin, W. and Ulbricht, M., 2020. Thinking the future of membranes: Perspectives for advanced and new membrane materials and manufacturing processes. *Journal of Membrane Science*, 598, p.117761.
- 66- Bhol, P., Yadav, S., Altaee, A., Saxena, M., Misra, P.K. and Samal, A.K., 2021. Graphene-based membranes for water and wastewater treatment: a review. *ACS Applied Nano Materials*, 4(4), pp.3274-3293.
- 67- Qi, R., Wang, Y., Li, J. and Zhu, S., 2006. Sulfur removal from gasoline by pervaporation: The effect of hydrocarbon species. *Separation and purification technology*, 51(3), pp.258-264.
- 68- Wang, L., Zhao, Z., Li, J. and Chen, C., 2006. Synthesis and characterization of fluorinated polyimides for pervaporation of n-heptane/thiophene mixtures. *European polymer journal*, 42(6), pp.1266-1272. Wang, L., Zhao, Z., Li, J. and Chen, C., 2006. Synthesis and characterization of fluorinated polyimides for pervaporation of n-heptane/thiophene mixtures. *European polymer journal*, 42(6), pp.1266-1272.
- 69- Xu, R., Liu, G. and Dong, X., 2010. Pervaporation separation of n-octane/thiophene mixtures using polydimethylsiloxane/ceramic composite membranes. *Desalination*, 258(1-3), pp.106-111.
- 70- Lin, L., Wang, G., Qu, H., Yang, J., Wang, Y., Shi, D. and Kong, Y., 2006. Pervaporation performance of crosslinked polyethylene glycol membranes for deep desulfurization of FCC gasoline. *Journal of membrane science*, 280(1-2), pp.651-658.
- 71- Chen, J., Li, J., Chen, J., Lin, Y. and Wang, X., 2009. Pervaporation separation of ethyl thioether/heptane mixtures by polyethylene glycol membranes. *Separation and purification technology*, 66(3), pp.606-612.
- 72- Chen, J., Li, J., Chen, J., Lin, Y. and Wang, X., 2009. Pervaporation separation of ethyl thioether/heptane mixtures by polyethylene glycol membranes. *Separation and purification technology*, 66(3), pp.606-612.

- 73- Yang, Z., Zhang, W., Li, J. and Chen, J., 2012. Polyphosphazene membrane for desulfurization: Selecting poly [bis (trifluoroethoxy) phosphazene] for pervaporative removal of thiophene. *Separation and purification technology*, 93, pp.15-24.
- 74- Yang, Z.J., Wang, Z.Q., Li, J. and Chen, J.X., 2013. Enhancing FCC gasoline desulfurization performance in a polyphosphazene pervaporative membrane. *Separation and Purification Technology*, 109, pp.48-54.
- 75- Yu, S., Pan, F., Yang, S., Ding, H., Jiang, Z., Wang, B., Li, Z. and Cao, X., 2015. Enhanced pervaporation performance of MIL-101 (Cr) filled polysiloxane hybrid membranes in desulfurization of model gasoline. *Chemical Engineering Science*, 135, pp.479-488.
- 76- Yu, S., Jiang, Z., Ding, H., Pan, F., Wang, B., Yang, J. and Cao, X., 2015. Elevated pervaporation performance of polysiloxane membrane using channels and active sites of metal organic framework CuBTC. *Journal of Membrane Science*, 481, pp.73-81.
- 77- Chen, J., Li, J., Qi, R., Ye, H. and Chen, C., 2008. Pervaporation performance of crosslinked polydimethylsiloxane membranes for deep desulfurization of FCC gasoline: I. Effect of different sulfur species. *Journal of Membrane Science*, 322(1), pp.113-121.
- 78- Nedeljkovic, D., 2021. Application of poly (ether imide) membranes for the removal of the aromatic sulphur compounds from gasoline. *Materials Research Express*, 8(7), p.075307.
- 79- Samanta, M. and Mitra, D., 2023. Fabrication, characterization and performance analysis of different Ag/PVA nanocomposite membranes for debenzenation of model pyrolysis gasoline using pervaporation. *Composite Interfaces*, pp.1-21.
- 80- Wang, L., Wang, Y., Wu, L. and Wei, G., 2020. Fabrication, properties, performances, and separation application of polymeric pervaporation membranes: A review. *Polymers*, 12(7), p.1466.
- 81- Yong, W.F. and Zhang, H., 2021. Recent advances in polymer blend membranes for gas separation and pervaporation. *Progress in Materials Science*, 116, p.100713.
- 82- Rostovtseva, V., Pulyalina, A., Rudakova, D., Vinogradova, L. and Polotskaya, G., 2020. Strongly selective polymer membranes modified with heteroarm stars for the ethylene glycol dehydration by pervaporation. *Membranes*, 10(5), p.86.
- 83- Arslan, M., Acik, G. and Tasdelen, M.A., 2019. The emerging applications of click chemistry reactions in the modification of industrial polymers. *Polymer Chemistry*, 10(28), pp.3806-3821.
- 84- Gongping, L.I.U., Wang, W.E.I., Wanqin, J.I.N. and Nanping, X.U., 2012. Polymer/ceramic composite membranes and their application in pervaporation process. *Chinese Journal of Chemical Engineering*, 20(1), pp.62-70.

- 85- Mavukkandy, M.O., McBride, S.A., Warsinger, D.M., Dizge, N., Hasan, S.W. and Arafat, H.A., 2020. Thin film deposition techniques for polymeric membranes—A review. *Journal of Membrane Science*, 610, p.118258.
- 86- Li, Y.J., Fan, C.Y., Zhang, J.P. and Wu, X.L., 2018. A promising PMHS/PEO blend polymer electrolyte for all-solid-state lithium ion batteries. *Dalton transactions*, 47(42), pp.14932-14937.
- 87- Zhai, H. and Rubin, E.S., 2013. Techno-economic assessment of polymer membrane systems for postcombustion carbon capture at coal-fired power plants. *Environmental science & technology*, 47(6), pp.3006-3014.
- 88- Chen, J., Li, J., Qi, R., Ye, H. and Chen, C., 2008. Pervaporation performance of crosslinked polydimethylsiloxane membranes for deep desulfurization of FCC gasoline: I. Effect of different sulfur species. *Journal of Membrane Science*, 322(1), pp.113-121.
- 89- Dai, W., Wang, H., Yuan, X.Z., Martin, J.J., Yang, D., Qiao, J. and Ma, J., 2009. A review on water balance in the membrane electrode assembly of proton exchange membrane fuel cells. *International Journal of hydrogen energy*, 34(23), pp.9461-9478.
- 90- Kong, Y., Lin, L., Zhang, Y., Lu, F., Xie, K., Liu, R., Guo, L., Shao, S., Yang, J. and Shi, D., 2008. Studies on polyethylene glycol/polyethersulfone composite membranes for FCC gasoline desulphurization by pervaporation. *European Polymer Journal*, 44(10), pp.3335-3343.
- 91- Kong, Y., Lin, L., Zhang, Y., Lu, F., Xie, K., Liu, R., Guo, L., Shao, S., Yang, J. and Shi, D., 2008. Studies on polyethylene glycol/polyethersulfone composite membranes for FCC gasoline desulphurization by pervaporation. *European Polymer Journal*, 44(10), pp.3335-3343.
- 92- Inaba, M., Kinumoto, T., Kiriake, M., Umebayashi, R., Tasaka, A. and Ogumi, Z., 2006. Gas crossover and membrane degradation in polymer electrolyte fuel cells. *Electrochimica Acta*, 51(26), pp.5746-5753.
- 93- Lin, L., Kong, Y., Wang, G., Qu, H., Yang, J. and Shi, D., 2006. Selection and crosslinking modification of membrane material for FCC gasoline desulfurization. *Journal of Membrane Science*, 285(1-2), pp.144-151.
- 94- Jiang, C. and Hou, Y., 2023. Polymer Membrane Based Pervaporation Process for Separating Organic Mixture by Molecular Simulation. *Macromolecular Chemistry and Physics*, p.2300069.
- 95- Bhattacharya, A., Tondon, P. and Jain, M., 2022. Modeling and simulations of plate and frame pervaporative module for the production of low sulfur containing FCC gasoline. *Materials Today: Proceedings*, 50, pp.146-149.
- 96- Vane, L.M., 2022. Effect of membrane performance variability with temperature and feed composition on pervaporation and vapor permeation system design for solvent drying. *Journal of Chemical Technology & Biotechnology*, 97(10), pp.2706-2719.

- 97- Vatankhah, F., Moheb, A. and Mehrabani-Zeinabad, A., 2021. A study on the effects of feed temperature and concentration on design of a multi-stage pervaporation system for isopropanol-water separation using commercial available modules with inter-stage heating. *Journal of Membrane Science*, 618, p.118717.
- 98- Bowen, T.C., Noble, R.D. and Falconer, J.L., 2004. Fundamentals and applications of pervaporation through zeolite membranes. *Journal of Membrane Science*, 245(1-2), pp.1-33.
- 99- Möller, M.N., Cuevasanta, E., Orrico, F., Lopez, A.C., Thomson, L. and Denicola, A., 2019. Diffusion and transport of reactive species across cell membranes. *Bioactive lipids in health and disease*, pp.3-19.
- 100-De Angelis, L. and de Cortalezzi, M.M.F., 2016. Improved membrane flux recovery by Fenton-type reactions. *Journal of Membrane Science*, 500, pp.255-264.
- 101-Jyoti, G., Keshav, A. and Anandkumar, J., 2015. Review on pervaporation: theory, membrane performance, and application to intensification of esterification reaction. *Journal of Engineering*, 2015.
- 102-Soares, L.S., Vieira, A.C.F., Fidler, F., Fritz, A.R.M. and Di Luccio, M., 2020. Pervaporation as an alternative for adding value to residues of oyster (*Crassostrea gigas*) processing. *Separation and Purification Technology*, 232, p.115968.
- 103-Galiano, F., Castro-Muñoz, R. and Figoli, A., 2021. Pervaporation, vapour permeation and membrane distillation: From membrane fabrication to application. *Membranes*, 11(3), p.162.
- 104-Grushevenko, E.A., Podtynnikov, I.A. and Borisov, I.L., 2019. High-selectivity pervaporation membranes for 1-butanol removal from wastewater. *Russian Journal of Applied Chemistry*, 92, pp.1593-1601.
- 105-Vane, L.M., 2019. Membrane materials for the removal of water from industrial solvents by pervaporation and vapor permeation. *Journal of Chemical Technology & Biotechnology*, 94(2), pp.343-365.
- 106-Li, N.N., Fane, A.G., Ho, W.W. and Matsuura, T. eds., 2011. *Advanced membrane technology and applications*. John Wiley & Sons.
- 107-Battal, T., Baç, N. and Yilmaz, L., 1995. Effect of feed composition on the performance of polymer-zeolite mixed matrix gas separation membranes. *Separation science and technology*, 30(11), pp.2365-2384.
- 108-Wu, J., Yuan, X.Z., Martin, J.J., Wang, H., Zhang, J., Shen, J., Wu, S. and Merida, W., 2008. A review of PEM fuel cell durability: Degradation mechanisms and mitigation strategies. *Journal of Power Sources*, 184(1), pp.104-119.
- 109-Zhao, C., Li, J., Qi, R., Chen, J. and Luan, Z., 2008. Pervaporation separation of n-heptane/sulfur species mixtures with polydimethylsiloxane membranes. *Separation and purification technology*, 63(1), pp.220-225.

- 110-LaConti, A.B., Hamdan, M. and McDonald, R.C., 2003. Mechanisms of membrane degradation. Handbook of fuel cells, 3, pp.647-662.
- 111-Soukane, S., Naceur, M.W., Francis, L., Alsaadi, A. and Ghaffour, N., 2017. Effect of feed flow pattern on the distribution of permeate fluxes in desalination by direct contact membrane distillation. Desalination, 418, pp.43-59.
- 112-Gu, B., Adjiman, C.S. and Xu, X.Y., 2017. The effect of feed spacer geometry on membrane performance and concentration polarisation based on 3D CFD simulations. Journal of Membrane Science, 527, pp.78-91.
- 113-Wu, Y., Meng, D., Yao, D., Liu, X., Xu, Y., Zhu, Z., Wang, Y. and Gao, J., 2020. Mechanism analysis, economic optimization, and environmental assessment of hybrid extractive distillation–pervaporation processes for dehydration of n-propanol. ACS Sustainable Chemistry & Engineering, 8(11), pp.4561-4571.
- 114-Zheng, P., Li, C., Wang, N., Li, J. and An, Q., 2019. The potential of pervaporation for biofuel recovery from fermentation: An energy consumption point of view. Chinese Journal of Chemical Engineering, 27(6), pp.1296-1306.